# 16-CHEM-A1, PROCESS BALANCES and CHEMICAL THERMODYNAMICS

#### **MAY 2019**

## **Three Hours Duration**

#### **NOTES:**

- 1) If doubt exists as to the interpretation of any question, you are urged to submit a clear statement of any assumptions made along with the answer paper.
- 2) Property data required to solve a given problem are provided in the problem statement or are available in the recommended texts. If you are unable to locate the required data, do not let this prevent you from solving the rest of the problem. Even in the absence of property data, you still have the opportunity to provide a solution methodology.
- 3) This is an open-book exam. Any non-communicating calculator is permitted.
- 4) The examination is in two parts Part A (Questions 1 to 3): Process Balances Part B (Questions 4 and 6): Chemical Thermodynamics
- 5) Answer TWO questions from Part A and TWO questions from Part B.
- 6) FOUR questions constitute a complete paper.
- 7) Each question is of equal value.

# PART A: PROCESS MASS and ENERGY BALANCES

- An air-conditioning plant is used to maintain a dry-bulb temperature of 27 °C and relative humidity of 50% in an auditorium. The air flow rate to the auditorium is 20,900 m³/hr at a dry-bulb temperature of 17 °C and relative humidity of 83.5%. The effluent air from the auditorium is partially recycled and mixed with the incoming fresh air, which is fed at a rate of 4,500 m³/hr at a dry-bulb temperature of 35 °C and relative humidity of 70%. The mixed air, which has a dry-bulb temperature of 29.5 °C and relative humidity of 54%, is passed through the air-conditioning plant to make it suitable for feeding to the auditorium. The total pressure can be assumed to be constant at 1 atm (101.325 kPa).
  - (a) [11 points] Calculate the moisture removed in the air-conditioning plant.
  - (b) [3 points] Calculate the moisture added in the auditorium.
  - (c) [11 points] Calculate the recycle ratio (moles of air recycled per mole of input fresh air)

#### DATA:

Absolute molar humidity of fresh air at 35 °C =  $4.05 \times 10^{-2}$  moles per mole of dry air

Absolute molar humidity of mixed air at 29.5 °C =  $2.25 \times 10^{-2}$  moles per mole of dry air

Absolute molar humidity of air entering the auditorium at  $17 \, ^{\circ}\text{C} = 1.63 \times 10^{-2}$  moles per mole of dry air

Absolute molar humidity of air leaving the auditorium at 27 °C =  $1.81 \times 10^{-2}$  moles per mole of dry air

A mixture containing 75% iron pyrite (FeS<sub>2</sub>) ore and 25% zinc sulfide (ZnS) ore by weight are burnt in burner. The pyrites yield 92% FeS<sub>2</sub> and the rest is gangue. The zinc sulfide ore contains 68% ZnS and the rest are inerts. A sample of the cinder product yields 3.5% sulfur with 70% of the sulfur in the cinder in the form of SO<sub>3</sub> absorbed in it and the rest is unoxidized FeS<sub>2</sub>. The stochiometrically unbalanced reactions in the burner are as follows:

$$FeS_2 + O_2 \rightarrow Fe_2O_3 + SO_2$$

$$FeS_2 + O_2 \rightarrow Fe_2O_3 + SO_3$$

$$ZnS + O_2 \rightarrow ZnO + SO_2$$

- (a) [20 points] Calculate the amount of cinder product formed and its composition based on 100 kg of mixed charge to the burner.
- (b) [5 points] Calculate the percentage of sulfur left in the cinder product based on the total sulfur charged.

A sulfur burner in a sulfite pump mill burns 200 kg of pure sulfur per hour. The gas leaves the burner at 871 °C and they are cooled before being sent to an absorption tower. As a primary cooler, a waste heat boiler is employed for producing saturated steam at a pressure of 15 bars (absolute). The feed water to the boiler is available at 183 °C and the temperature of the gas mixture leave the boiler is 190 °C. Calculate the amount of steam produced in kg per hour assuming 10% excess air, 90% efficiency, complete combustion, no heat loss to the surroundings and no SO<sub>3</sub> formation.

#### DATA:

Standard molar specific heat capacity of SO<sub>2</sub> in kJ/kmol.K =  $24.7706 + 62.9841 \times 10^{-3} \text{ T} - 4.42582 \times 10^{-5} \text{ T}^2 + 11.122 \times 10^{-9} \text{ T}^3$ 

Standard molar specific heat capacity of  $O_2$  in kJ/kmol.K =  $26.0257 + 11.7551 \times 10^{-3} T - 2.3426 \times 10^{-6} T^2 - 56.23 \times 10^{-11} T^3$ 

Standard molar specific heat capacity of  $N_2$  in kJ/kmol.K = 29.5909 + 51.141 x  $10^{-4}$  T - 1.31829 x  $10^{-5}$  T<sup>2</sup> - 49.68 x  $10^{-10}$  T<sup>3</sup>

Saturation temperature of steam at 15 bars pressure = 198 °C

Latent heat of vaporization of water at 15 bars pressure = 1945 kJ/kg

Specific heat capacity of water = 4.1868 kJ/kg.K

# PART B: CHEMICAL THERMODYNAMICS

- Water gas, available at a temperature of 500 °C and a pressure 4 bar, has the following composition: 70.4 grams of hydrogen, 23.68 grams of methane, 35.84 grams of ethylene, 66 grams of carbon dioxide, 94.92 grams of carbon monoxide and 50.4 grams of nitrogen.
  - (a) [5 points] Calculate the volume of water gas if it behaves as an ideal gas.
  - (b) [20 points] Calculate the volume of water gas if it follows van der Waals equation of state.

### DATA:

Component	Formula	Critical Temperature (K)	Critical Pressure (bar)
Hydrogen	H <sub>2</sub>	32.2	12.97
Methane	CH <sub>4</sub>	190.56	45.99
Ethylene	C <sub>2</sub> H <sub>4</sub>	282.34	50.41
Carbon Monoxide	СО	132.91	34.99
Carbon Dioxide	CO <sub>2</sub>	304.1	73.75
Nitrogen	N <sub>2</sub>	126.9	33.94

Pyrites are roasted in a roaster plant for making sulfuric acid. The gases leave the roaster at 502 °C with the mass composition: 3.57% SO<sub>2</sub>, 1.08% O<sub>2</sub>, 0.18% SO<sub>3</sub> and the rest N<sub>2</sub>. Calculate the heat content of 1 kmol of gas mixture over 25 °C.

### DATA:

Standard molar specific heat capacity of SO<sub>2</sub> in kJ/kmol.K = 24.7706 + 62.9841 x  $10^{-3}$  T - 4.42582 x  $10^{-5}$  T<sup>2</sup> + 11.122 x  $10^{-9}$  T<sup>3</sup>

Standard molar specific heat capacity of  $O_2$  in kJ/kmol.K =  $26.0257 + 11.7551 \times 10^{-3} \text{ T} - 2.3426 \times 10^{-6} \text{ T}^2 - 56.23 \times 10^{-11} \text{ T}^3$ 

Standard molar specific heat capacity of SO<sub>3</sub> in kJ/kmol.K =  $22.0376 + 12.1624 \times 10^{-2} \text{ T} - 9.18673 \times 10^{-5} \text{ T}^2 - 24.3691 \times 10^{-9} \text{ T}^3$ 

Standard molar specific heat capacity of  $N_2$  in kJ/kmol.K = 29.5909 + 51.141 x  $10^{-4}$  T - 1.31829 x  $10^{-5}$  T<sup>2</sup> - 49.68 x  $10^{-10}$  T<sup>3</sup>

3) 2 moles of methane (CH<sub>4</sub>) and 3 moles of water react and gaseous mixture containing CH<sub>4</sub>, H<sub>2</sub>O, CO, CO<sub>2</sub> and H<sub>2</sub> is obtained. Calculate the equilibrium composition of the mixture at 1000 K and 1 atmosphere.

### DATA:

Standard Gibbs free energy of formation of CH<sub>4</sub> at 1000 K = 19.3 kJ/mole Standard Gibbs free energy of formation of H<sub>2</sub>O at 1000 K = - 192.72 kJ/mole Standard Gibbs free energy of formation of CO at 1000 K = - 200.715 kJ/mole Standard Gibbs free energy of formation of CO<sub>2</sub> at 1000 K = - 396.11 kJ/mole Standard Gibbs free energy of formation of H<sub>2</sub> at 1000 K = 0 kJ/mole

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	17	Fluorine 9 <b>F</b> 19.00	CI CI 35.45		Bromine 35	ā	79.90	lodine 53	- 8	126.90	Astaline 85	Αt	(210)	Unursepium 117	Ous	(2947)
	16	Oxygen 8 O	Suffer 16 S 32.07		Selenium 34	Se	78.96	Tellurium 52	Te	127.60	Polonium 84	Ъ	(209)	Ununhexium 116	Unh	(293)
	15	Nitrogen 7 N N 14.01	Phosphorus 15 P 30.97		Arsenic 33	As	74.92	Antimony 51	Sb	121.76	Bismuth 83	ö	208.98	Ununpentium 115	Uup	(288)
	4	C C 12.01	Silicon 14 Si 28.09		Germanium 32	Ge	72.61	_i 20	Sn	118.71	Lead 82	Pb	207.20	Ununquadium 114	Dnd	(289)
ol .	13	Boron 5 5	Aluminum 13 <b>A</b> I 26.98		Galfium 31	Ga	69.72	Indium 49	드	114.82	Thallium 61	F	204.38	Ununtrium 113	Uut	(284)
	#	Mass		12	2Inc 30	Zu	65.39	Cadmium 48	g	112.41	Mercury 80	H	200.59	Copernicium 112	ပ်	(285)
7	Atomic #	— Avg. Mass		7	Copper 29	٦ ک	63.55	Silver 47	Ag	107.87	Gold 79	Αn	196.97	Roentgenium 111	Rg	(280)
	only O ¢	<b>5</b> 9 ↔		10	Nickel 28	Z	58.69	Palladium 46	Pd	106.42	Platinum 78	<u>7</u>	195.08	Darmstadtium 110	Ds	(281)
200	<ul> <li>✓ Mercury</li> <li>№</li> </ul>	200.59		o	Cobail 27	ဝိ	58.93	Rhodium 45	R	102.91	lridium 77	<u>=</u>	192.22	Meitnerlum 109	Mt	(276)
2	me pol		-::	œ	Iron 26	Fe	55.85	Rutherium 44	Ru	101.07	Osmium 76	ő	190.23	Hassium 108	Hs	(270)
	Element name.			7	Manganese 25	Mn	54.94	Technelium 43	Тc	(86)	Rhenium 75	Re	186.21	Bohrium 107	Bh	(272)
	E			9	Chromium 24	င်	52.00	Molybdenum 42	Mo	95.94	Tungsten 74	>	183.84	Seaborgium 106	Sg	(271)
D#5	netals als ni-metal)			S	Vanadium 23	>	50.94	Niobium 41	qN	92.91	Tantalum 73	Ta	180.95	Dubnium 105		
	Alkali metals Alkaline earth metals Transition metals Other metals Metalloids (semi-metal)	Nonmetals Halogens Noble gases		4	Titanium 22	F	47.88	Zirconium 40	Zr	91.22	Hafnium 72	Ŧ	178.49	Rutherfordium 104	Ŗ	(267)
	Alka Trai	N H N		က	Scandium 21	Sc	44.96	7tmum 39	>	88.91	Lutetium 71	Γn	174.97	Lawrencium 103	בֿ	(262)
											57-70	*		89,102	*	
	8	Beryllium 4 Be 9.01	Magnesium 12 Mg 24.31		Calcium 20	Ca	40.08	Stronlium	Sr	87.62	Barium 56	Ba	137.33	Radium 88	Ra	(226)
۳	Hydrogen 1.01	Lithium 3 Li 6.94	11 Na 22.99	9.	Potassium 19	¥	39.10	Rubidium 37	Rb	85.47	Cesium 55	Cs	132.91	Francium 87	Ţ	(223)

*lanthanides	Lanthanum 57 La 138.91	Cenum 58 Ce 140.12	Praseodymium 59 Pr 140.91	Neodymium 60 <b>Nd</b> 144.24	Promethium 61 Pm (145)	Samanum 62 <b>Sm</b> 150.36	Europium 63 <b>Eu</b> 151.97	Gadolinium 64 Gd 157.25	Terbium 65 Tb 158.93	Dy 162.50	Holmium 67 HO 164.93	68 68 <b>Er</b> 167.26	Thulium 69 Tm 168.93	Ytterbum 70
**actinides	Actinium 89 AC (227)	Thorium 90 Th 232.04	Protactinium 91 Pa 231.04	U 238.03	93 Np (237)	Plutonium 94 Pu (244)	Americium 95 Am (243)	Curium 96 Cm (247)	97 BK (247)	Saiffornium 98 Cf (251)	99 Es Es	Fermium 100 Fm (257)	Mendelevium 101 Md (258)	Nobelium 102 No (259)